



A parabolic trough solar collector as a solar system for heating water: a study based on numerical simulation

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Abstract – This paper is an optical and thermal study of a small model of a parabolic trough solar collector (CTP), which will be used to heat tap water, in the winter, at Guemar location, (El-Oued, Algeria). A mathematical model was presented based on the energy balance equation applied to the absorber tube; this model was solved by the finite difference method. A computer program based on MATLAB was developed to solve the problem. The results show that the thermal efficiency of the concentrator can attend a high value of more than 61%, while the fluid outlet temperature can reach 343 K.

Keywords: Solar thermal, parabolic trough collector, outlet temperature, Tap water, numerical analysis.

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I. Introduction

The oldest and the greatest source of energy in the universe is the sun, where an average of 1367 (W/m²) reached the edge external of the terrestrial atmosphere according to the world radiometric center of Davos (Switzerland) [1].

The global solar radiation is the sum of both direct and diffuse components [2-16]. Algeria has one of the highest solar radiation in Africa. The sunshine duration on almost all of the national territory exceeds 2000 hours annually and can reach 3900 hours in the Highlands and Sahara [17].

This study deals with the exploitation of solar energy to produce hot water using parabolic trough concentrator (PTC) in Guemar region, where the table (1) shows the meteorological data of this city. In previous studies, we have studied several models of this system in different regions in Algeria, where the results were very encouraging [2-11].

Table 1. The meteorological data of the city of Guemar.

Month	Global Radiation (kWh/m ²)	Diffuse Radiation (kWh/m ²)	Beam Radiation (kWh/m ²)	Monthly average of ambient temperature (°C)	Monthly average of dew point (°C)	Monthly average of wind speed (m/s)
1	114	19	211	10,6	4	2,1
2	125	28	184	12,9	3,1	2,5
3	170	48	197	17,8	4,6	3,3
4	207	54	225	21,6	7,1	4
5	234	69	237	26,8	9,6	4,1
6	236	70	228	31,3	11,4	3,6
7	248	66	242	34,7	13,3	3,4
8	219	67	217	33,8	14,6	3,1
9	176	55	187	28,8	15	3
10	144	45	179	23,8	12,7	2,2
11	117	21	200	16,1	7,3	2
12	100	21	187	11,7	5,1	2,3

For the PTC solar concentrator, it gives us a temperature of fluid that can be used both in industrial and domestic applications, with a medium- to high range

of [80-160 ° C] [2-6, 9, 11]. According to the size and position of the PTC collector, this system can obtain a steam temperature exceeding 1500 °C, according to

studies cited in the scientific literature [3-6, 9, 11, 18]. So, the PTC systems are the most currently used technology by the most powerful solar power plants in the world, we quote in this context that the solar plant at Kramer Junction in California represents a total installed capacity of 354 MW [19]. This kind of solar field is made up of parallel alignments of long half-cylindrical mirrors, oriented North-South axis that revolved around the latter to follow the path of the Sun. The Sun's rays are concentrated on a horizontal tube, where circulates a heat transfer fluid.

As we said earlier, this study focuses on the conversion of solar energy to thermal energy by using a parabolic trough solar concentrator in a troubled day of the winter (Low-temperature weather with some wind). Tap water was used as the heat transfer fluid. Our aim in this study is to characterize the optical and thermal efficiencies of our PTC model based on the geographic parameters and climatic conditions in Guemar location, (El-Oued, Algeria). Figure 1 shows the scheme of the approved water heating system using TRNSYS 16.

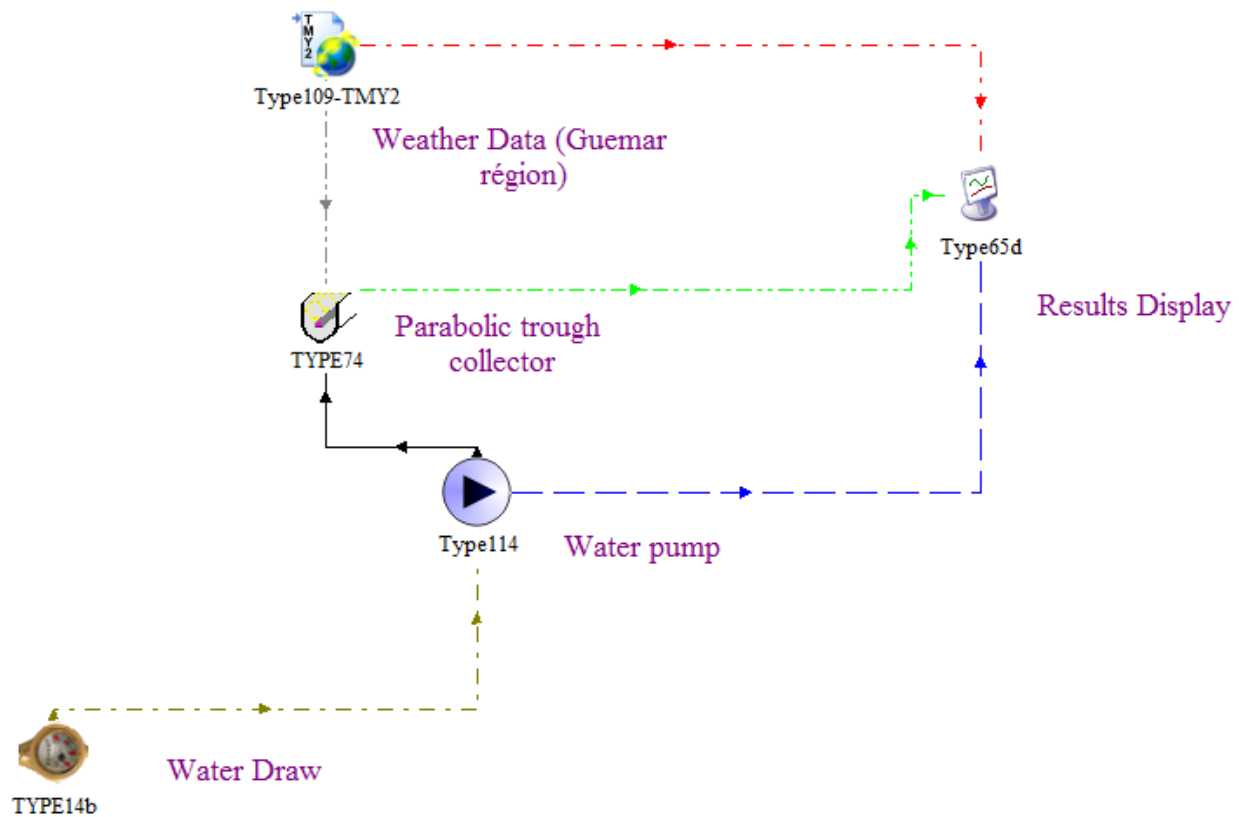


Figure 1. Illustrative diagram of the water heater system.

In order to solve to problem, this study will begin with an optical efficiency analysis using SolTrace software. In the second step, a mathematical model has been established with Matlab to calculate the thermal efficiency, the fluid outlet temperature, the receiver's surface temperature, the glass temperature and the coefficient of thermal losses.

II. Optical simulation

The optical modeling was performed using the SolTrace; the code is developed by the National Renewable Energy Laboratory (USA) [20]. The optical system of the concentrator is composed of the reflecting surface and absorber tube. The reflecting surface was modeled as a single mirror of parabolic section. Table (2) shows the geometric parameters of the PTC concentrator and the optical parameters are shown in Table (3).

Table 2. Geometrical parameters of the PTC collector.

geometric characteristic	Value (mm)
Receiver tube number	1
Absorber length (L_A)	12270
outer diameter of the absorber ($D_{A,ext}$)	22
Inner diameter of the absorber ($D_{A,int}$)	20
outer diameter of the glass ($D_{V,ext}$)	26
inner diameter of the glass ($D_{V,int}$)	23,5
mirror length (L)	12270
mirror width (l)	1100

The absorbent tube dimensions mentioned in the previous table are the dimensions of a linear Fresnel receiver that was previously manufactured by H. Chabahi et al., (2011) [21], but the length of the absorbent tube here was different.

For the optical simulation, it was assumed that the reflection coefficient, the absorptivity, and transmissivity are uniform over the entire reflecting surface. It was considered that the solar tracking is very accurate and therefore the concentrator opening is constantly perpendicular to the rays from the solar disc.

Table 3. Optical parameters of the collector.

parameter	Value
optical overall average error (σ_{optical})	03 mrad
mirror reflection coefficient (ρ_m)	0,92
Transmissivity of the glass	0,945
Absorption coefficient of the absorber (α)	0,94
The emissivity of the absorber tube (ε_A)	0,12

There are several models for the simulation of global direct and diffuse solar irradiance, expressed by semi-empirical approaches.

For the PTC concentrators, the absorbed solar energy depends on the beam radiation (DNI) [3-6, 9, 11]. Figure 2 reflects the change in the solar radiation during the day of 05 December 2016 according to the semi-empirical model of PERRIN DE BRICHAMBAUT, where M. Ghodbane et al., (2016), had created a numerical simulation based on programming using MATLAB for the calculation of solar radiation (direct, diffuse and global) [8]. For this model, the different components of the solar radiation vary according to the height of the sun, the angle of incidence, the weather condition and the state of visibility of the atmosphere.

Any application of solar energy in a given site requires a complete and detailed knowledge of the sunshine of the site. This is possible if the data are available over a sufficient period. However, in the majority of cases, there are no local measurements of solar radiation, and some approximate methods must be used to predict the characteristics of solar irradiation.

The total quantity of radiation calculated for a particular location or area was entered as global radiation. The calculation radiation (direct, diffuse and global) was repeated for each entity location or for all locations of the topographic surface and generates sunshine maps for an entire geographical area.

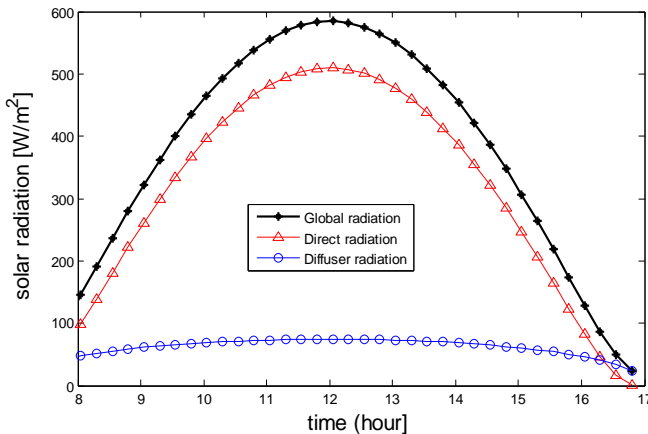


Figure 2. Solar radiation evaluation in Guemar area.

Virtually, it was in the regions for which we had the least solar radiation measurements that the projects of implantation of the solar energy systems for water pumping, desalination, or the decentralized electric power supply are the most important and the most demanding. Direct radiation (DNI) is solar radiation reaching the earth's surface directly from the sun. It depends on the thickness of the atmosphere that the solar radiation must cross, as well as the inclination of the rays relative to the ground. The PYRHELIOMETER is the instrument for measuring the intensity of direct radiation. The PYRHELIOMETER must be equipped with a device to direct it permanently towards the sun. Through Figure 2, it was noticeable that the maximum radiation value is the true solar noon, which can reach 585 (W/m²), despite the bad weather on this day, the amount of solar radiation was considered.

Figure 3 illustrates the captured solar energy by the collector, as presented in SolTrace. We tried to show the importance and effectiveness of parabolic trough collector in the field of solar concentrate.

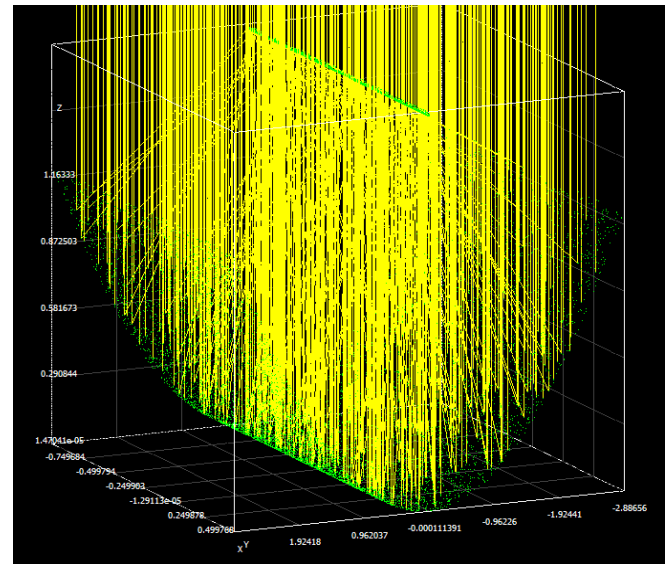


Figure 3. Schema parabolic trough concentrator as it appears in SolTrace.

III. Thermal simulation

This section treats the thermal analysis and numerical modeling of a PTC concentrator. This modeling was used to predict the change in the outlet temperature of the heat transfer fluid (water) versus the beam radiation. The thermal exchanges are between the heat transfer fluid, the absorber tube and the glass tube. The temperature modeling was based on the energy balances characterized by the differential equations of the three temperatures: T_F (for the fluid), T_V (for glass tube) and T_A (for the absorber tube), these equations will vary depending on

two parameters, namely the time (t) and the length (x) of the absorber tube. In calculating the energy balances, we have assume that [9, 13]:

- The heat transfer fluid is incompressible;
- The parabolic shape is symmetrical;
- The ambient temperature around the concentrator is uniform;
- The shadow effect of the absorber tube on the mirror is negligible;
- The solar flux at the absorber is uniformly distributed;
- The glass is considered opaque to infrared radiation;
- The exchanges by conduction in the absorber and the glass are negligible.

III.1. Energy balance for the fluid

The energy balance for the heat transfer fluid that circulates in the absorber tube was expressed by the following relationship [2, 5, 7, 10, 11]:

$$\rho_F \cdot C_F \cdot A_{A,int} \cdot \frac{\partial T_F(X,t)}{\partial t} = q_u - \rho_F \cdot C_F \cdot Q_v \cdot \frac{\partial T_F(X,t)}{\partial X} \quad (1)$$

The initial conditions and the boundary conditions of equation (1) are [2, 5, 10, 11]:

$$\begin{aligned} T_F(0,t) &= T_{F,entry}(t) = T_{amb}(t) \\ T_F(X,t) &= T_{F,initial}(t) = T_{amb}(0) \end{aligned} \quad (2)$$

q_u is the heat flow transmitted to the fluid [W]; it was given by the following relationship [3, 10, 14]:

$$q_u = h_F \cdot A_{A,int} (T_A - T_F) \quad (3)$$

III.2. Energy balance for the absorber tube

The energy balance for the absorber was given by the following equation [2, 5, 7, 10, 11]:

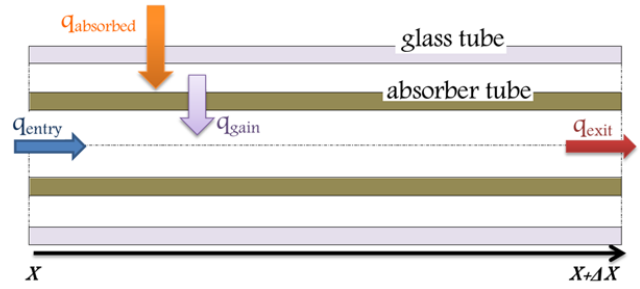
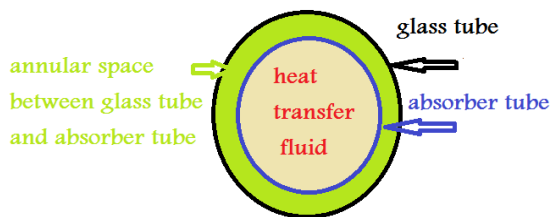


Figure 4. Thermal balance on a surface element of the parabolic cylindrical concentrator [3].

$$\rho_A \cdot C_A \cdot A_A \cdot \frac{\partial T_A(X,t)}{\partial t} = q_{absorbed}(t) - q_{exit}(X,t) - q_u(X,t) \quad (4)$$

The initial conditions for the equation (4) are [5, 10, 11]:

$$T_A(X,t) = T_{A,initial}(t) = T_{amb}(0) \quad (5)$$

III.3. Energy balance of the glass

Similarly, the energy balance for the glass was given by [2, 5, 7, 10, 11]:

$$\rho_V \cdot C_V \cdot A_V \cdot \frac{\partial T_V(X,t)}{\partial t} = q_{int}(X,t) - q_{ext}(X,t) \quad (6)$$

The initial condition of equation (6) is [5, 10, 11]:

$$T_V(X,t) = T_{V,initial}(t) = T_{amb}(0) \quad (7)$$

To solve this problem, we chose the finite difference method. A calculation program Matlab was established, after the discretization of non-linear equations that allowed us to obtain a set of numerical results.

The thermal power emitted by the sun and received by the concentrator is therefore [5, 10, 11, 22]:

$$q_{absorbed} = \rho_m \cdot \gamma \cdot A_c \cdot K_{cam} \cdot DNI \quad (8)$$

Where K_{cam} is Angle of incidence correction factor modified, γ is the intercept factor.

We can express the optical efficiency (η_{opt}) of the concentrator [5, 10, 11, 15]:

$$\eta_{opt} = \alpha \cdot \rho_m \cdot \gamma \cdot K_{cam} \quad (9)$$

The thermal efficiency (η) was calculated as follows [2,

5, 10, 11, 15]:

$$\eta = \eta_{opt} - \frac{U_L \cdot A_A \cdot (T_A - T_{amb})}{DNI \times A_C} \quad (10)$$

III.4. The coefficient of thermal losses

The coefficient of thermal losses (U_L) was expressed as [2, 5, 7, 10, 11]:

$$U_L = \left(\frac{1}{C_1 \left[\frac{T_A - T_{amb}}{1 + f} \right]^{0.25} + \frac{D_{A,int}}{D_{A,ext} \times h_v}} \right)^{-1} + \frac{\sigma(T_A^2 + T_{amb}^2) \cdot (T_A + T_{amb})}{\left[\varepsilon_A - 0.04(1 - \varepsilon_A) \left(\frac{T_A}{450} \right) \right]^{-1} - \left[\left(\frac{D_{A,int}}{D_{A,ext}} \right) \left(\frac{1}{\varepsilon_v} \right) \left(\frac{f}{\varepsilon_v} \right) \right]} \quad (11)$$

Where the factor (f) takes into account the loss ratio resulting from the wind, it can be obtained by the following equation [5, 10, 11]:

$$f = D_{A,int}^{-0.4} (1.61 + 1.3 \varepsilon_A) h_v^{-0.9} \times \exp[0.00325(T_A - 273)] \quad (12)$$

C_1 was given by the following empirical expression [5, 10, 11]:

$$C_1 = \frac{1.45 + 0.96(\varepsilon_A - 0.5)^2}{D_{A,int} \left(\frac{1}{D_{A,int}^{0.6} - D_{A,ext}^{0.6}} \right)^{1.25}} \quad (13)$$

The term (h_v) is the wind convection coefficient, it can be obtained by the following equation (according McAdams (1954)) [5, 10, 11, 15, 23]:

$$h_v = 5.7 + 3.8W_w \quad (14)$$

IV. Results and discussion

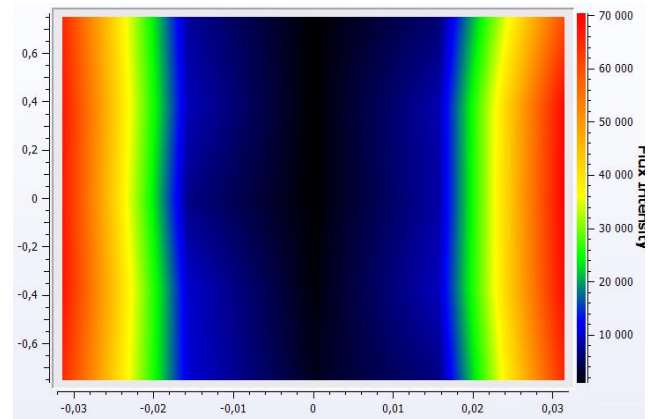
The PTC concentrators can offer an opportunity to sunny countries such as Algeria for investment and construction of solar central.

The right choice of the studied site is very important because each site is characterized by its direct illumination, the ambient temperature, the speed of the wind, the latitude, and the elevation compared to the level of the sea, which play a significant role on the profitability of the solar concentrator. These factors were quite apparent in the results obtained where the energy production vary when moving the solar collector in

different sites. We selected Guemar city to conduct this study, it is located at an altitude of 62 meters with a latitude and longitude of 33°29'24" N north and 06°47'50" East respectively. PTC concentrator had headed south. We chose tap water as the working fluid with a flow rate of 0.015 [kg/s].

The absorber was the seat of the thermal conversion (from concentrated solar radiation into high temperature heat sensitive). On wall of the absorber tube, the thermal energy acquired from the sun has propagated by direct contact of the particles without appreciable displacement of the latter. Figures 5a and 5b reflect the average intensities contours of heat flux on the absorber surface based on the direct solar radiation (DNI).

a) DNI= 1000 [W/m²]



b) DNI= 500 [W/m²]

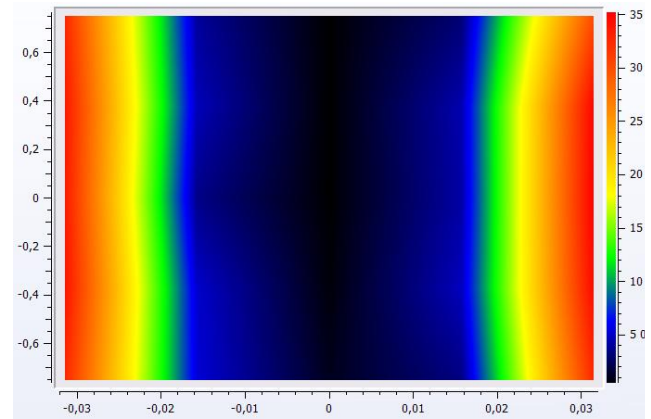


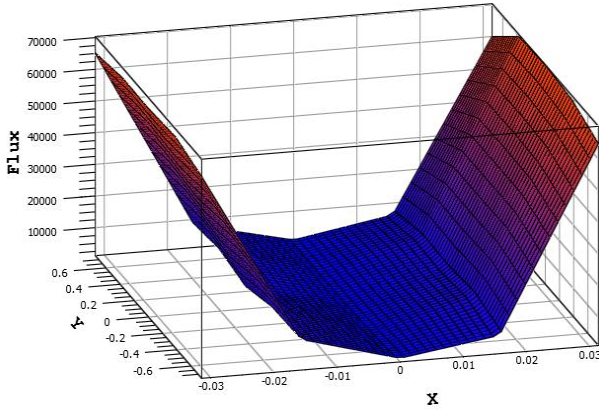
Figure 5. Flux intensity contour at the absorber tube [W/m²].

This assessment can approach the actual values of thermal flow influencing absorbers with a reflectivity of the mirrors equal to 92% and real illumination values. The main objective of the optical characterization have known the concentration of solar power on the surface absorber tube, and the evolution of the maximum value of thermal flow depending on the incidence angle of solar radiation.

Figures 6a and 6b illustrate the average heat flow distributions. We observe a good distribution of heat flux

at the surface level of the absorber. We can say that our concentrator has a good overall optical behavior. Thus, we can conclude that the average distributions of heat flux provided the software ray tracing issues representative of real flux distributions by the parabolic trough concentrator.

a) DNI= 1000 [W/m²]



b) DNI= 500 [W/m²]

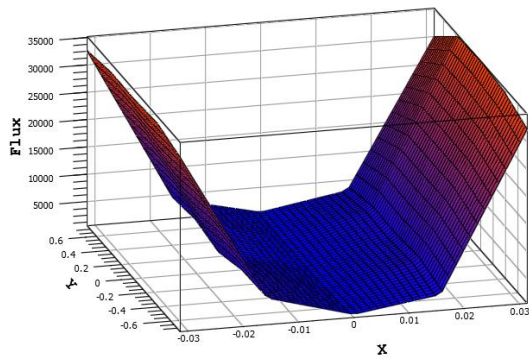


Figure 6. Flux intensity distribution at the absorber tube [W/m²].

Now we turn to the thermal analysis, the finite difference method was chosen to solve the non-linear equations of thermal balance. A calculation program using Matlab was developed after the discretization of the linear equations, which allowed us to obtain a set of numerical results, thus we will be able to know the performance of the concentrator. Figure 7 shows the evolution of optical performance versus time during the day of the study, while Figure 8 shows the evolution of thermal performance versus time for the same day.

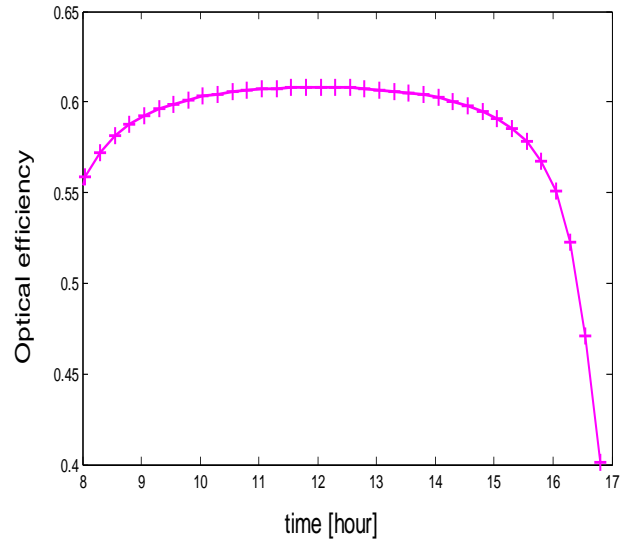


Figure 7. Evolution of optical efficiency.

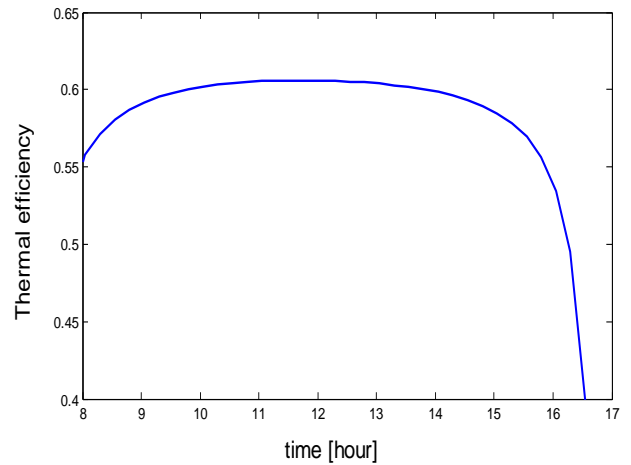


Figure 8. Thermal efficiency evolution versus the time.

It is noted that the thermal performance was equal to 60.61% at 12:00, after this time, the thermal efficiency decreases with the decreasing of solar radiation resources.

The receiver must absorb as much concentrated solar flux as possible, and convert it into thermal energy; this heat is transferred to water. The difference in temperature between the two faces (internal and external) of the absorber tube generates the creation of a heat flow. Figure 9 represents the variations of the absorber tube temperature, the fluid temperature and the glass temperature, where the wind speed (W_w) during the day was equal to 4.5 [m/s] and the water temperature inside the absorbent tube was equal to 9°C.

At the beginning of the day (at 08:00am), the temperature of the absorber tube was equal to the ambient temperature ($T_A = T_{amb} = 292K$), after one hour of heating this temperature increases according to the direct solar radiation concentrated to the absorber, it reaches 302 k. It continues to increase where its value becomes stationary. In this case, the absorber is in a state

of equilibrium, that is to say that all the surfaces of the absorber are at the same temperature, this state of equilibrium was very difficult to establish because of the influence of the wind. The maximum of the ambient temperature was reached between 12:00 and 14:00 hours, when the illumination is important.

The absorber tube is heated by concentrated direct solar radiation; this radiant energy absorbed by the absorber was converted into heat energy, which is transferred by convection to the water inside the receiver, which increases its temperature.

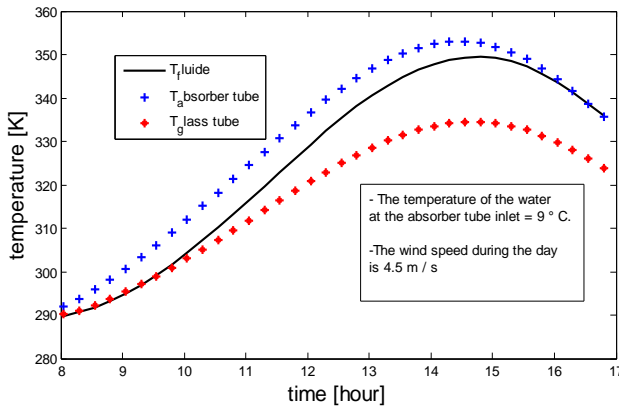


Figure 9. Evolution of the temperatures (T_A , T_F and T_V).

The heat transfer between the absorber tube and the water comes from the macroscopic movement of the water. According to figure 9, it is certain that the absorber tube temperature (T_A), the water temperature (T_F) and the glass temperature (T_V) were directly related to the experimental conditions of weather conditions.

The results in figure 9 show the rapid heating of water by solar irradiation during the day. It is noted that the temperature of the absorber (T_A) is close to (T_F) which it has the maximum value at 14:55, we recorded an absorber temperature equal to 353 (K), and this is a sign of a good thermal insulation and low heat loss between the absorber tube and the surrounding air. The selective surfaces are taking advantage of different wavelengths of incident solar radiation, so the selectivity of the surface will result in a maximum absorption in the solar and infrared spectrum minimum. Therefore, the absorber tube has a high absorptivity for visible solar radiation and low emissivity for the long's wavelength infrared radiation due to the selective coating of the absorber. This coating can retain the greater part of the incident solar energy on the surface of the absorber and lose very little amount of heat radiation in the wavelength when the absorbent surface becomes hot.

The decrease of the absorber tube surface results in an increase in the concentration, therefore the performances are higher. For a test day with a constant volumetric flow, the temperature depends mainly on the $q_{\text{absorbed}}(t)$, which is based on optical parameters, geometric of the concentrator and direct radiation received by the

collector.

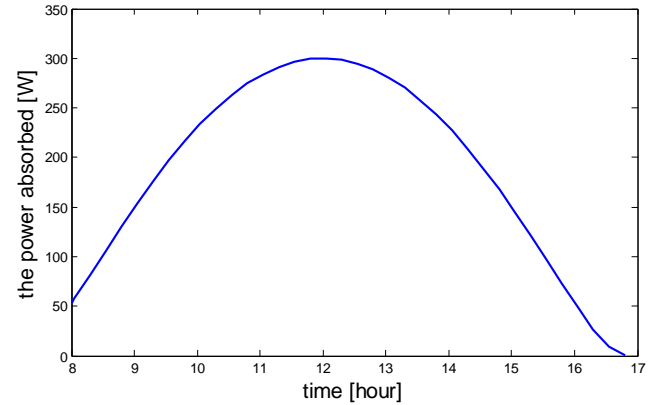


Figure 10. Evolution of the power absorbed.

The inside of the absorber absorbs infrared radiation, which undergoes a temperature increase (T_A) (greenhouse effect). Therefore, the temperature of the outer side is lower and close to the ambient medium subjected mainly to the wind speed, which creates convection to the outer side of the absorber, that is why the information about the meteorological data, including wind speed and ambient temperature are important parameters. The useful power absorbed by the receiver is used to heat the water inside the receiver and increases its temperature to a temperature of 353 k at 14:55.

In nature, there are three modes of heat transfer, thermal transfer by conduction, by convection (natural and / or forced) and by radiation. From these three modes of transfer results three types of thermal losses: thermal losses by conduction, by convection and finally by radiation. For the PTC solar concentrator, the heat losses are important because the temperature of the absorber tube is high. Moreover, these concentrators require regular maintenance to maintain the optical quality of the mirrors subjected to dust and corrosion of the environment. Figure 11 shows the variation in the coefficient of thermal losses as a function of the difference in temperature between the absorber tube and the ambient temperature ($T_A - T_{\text{amb}}$). In general, the heat loss coefficients depend on the insulation quality of PTC collector.

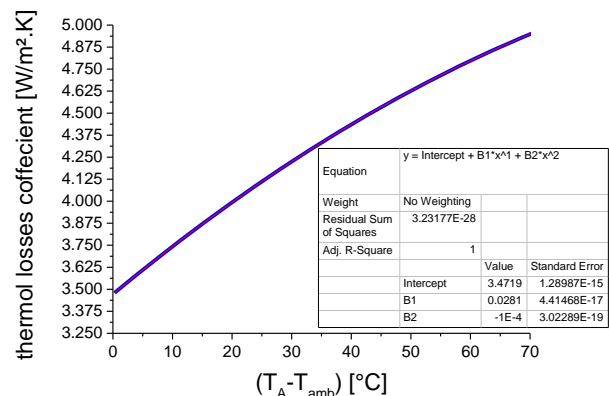


Figure 11. Evaluation of thermal losses coefficient.

It can be seen from figure 11 that the coefficients of global heat losses (U_L) increase slightly with increasing temperature. Thus, the coefficient of overall losses varies proportionally with the difference in temperature between the receiver tube and the ambient temperature ($T_A - T_{amb}$), and this is due to the amount of heat absorbed by the absorber. U_L increases with the increase of ($T_A - T_{amb}$), it varies from 3.4 to 5 W / m².K where 0° C < ($T_A - T_{amb}$) < 70 ° C. Therefore, we see that the coefficient of losses varies in a slightly slow way; this is due to the range of operating temperature that is not high, and also to the good thermal insulation of the receiver.

Generally, the climatic conditions vary from season to another (intensity of solar radiation and the ambient temperature) affect the productivity of hot water. Through our study on linear concentrator [3-6, 10, 11], we can conclude that the results are very encouraging to exploit and build fields of linear concentrators in all regions of the country (north, south, east and west).

V. Conclusion

This work is a numerical study of a parabolic trough concentrator (PTC) in a volatile day in the winter (Low air temperature with some wind). Tap water was used as heat transfer fluid. The study was based on the numerical analysis of the energy balance equations of the absorbent tube, the water and the glass envelope surrounding the absorbent tube. According to this numerical solution, we can control the absorber temperature, the fluid outlet temperature and the glass temperature. The thermal efficiency of device exceeds 61%, where the fluid temperature at outlet of the absorber tube is equal to 344 [K]. The results are very encouraging for the development of this type of solar concentrator in the country.

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Nomenclatures

\dot{V}	Volume flow rate (m ³ /s)
γ	Intercept factor
A_A	Absorber area (m ²)
A_c	Collector aperture area (m ²).
C_A	Specific heat of the absorber (J/kg k).
C_F	Specific heat of the fluid (J/kg k).
C_p	Thermal capacity (J/kg k).
$D_{A,ext}$	External diameter of the absorber (m).
$D_{A,int}$	Internal diameter of the absorber (m).
$D_{V,ext}$	External diameter of the glass tube (m).
$D_{V,int}$	Internal diameter of the glass (the transparent envelope) (m).
h_v	Coefficient of transfer by convection of the wind (W/m ² .K).
K_{cam}	Angle of incidence correction factor modified
$q_{absorbed}$	Heat absorbed in the absorber tube (W/m ²).
q_{exte}	Heat quantity lost to the outside (convection + conduction) between the glass and ambient (W/m ²).
q_{int}	Internal heat (convection + conduction) between the glass and ambient (W/m ²).
q_u	Heat exchanged by convection between the absorber and the fluid (W/m ²).
S_e	The effective area of a sensor reflector (m ²).
W_w	Wind velocity (m/s).
T_A	Temperature of the absorber (K).
T_{amb}	Ambient temperature (K).
T_F	Fluid temperature (K).
T_V	Temperature of the glass (K).
U_L	Overall coefficient of heat loss (W/m ² .K).
ϵ_A	Emissivity of the absorber tube
ϵ_V	Emissivity of the casing transparent glass
ρ_A	Density of the absorber (kg/m ³).
ρ_F	Fluid density (kg/m ³).
σ	Stefan-Boltzmann constant (W/m ² .K ⁴).